

HOMOGENEOUS PHOTOCATALYTIC DEGRADATION OF ACID ALIZARIN BLACK USING HYDROGEN PEROXIDE

Haydar A. Mohammad Salim, Sabir Ayob Mohammad Salih and Sherwan M. Simo

Dept. of Chemistry, Faculty of Science, University of Zakho, Kurdistan Region-Iraq.

(Accepted for publication: November 11, 2014)

ABSTRACT

Photocatalytic degradation of acid alizarin black (AAB) dye (C.I. 21725) in aqueous solution was investigated using UV light in the presence of hydrogen peroxide (H_2O_2) as a catalyst at different operating conditions. The operating conditions were concentration of catalyst dosage (0.1, 0.2 and 0.3 mL of 30 % H_2O_2), initial concentration of AAB dye (100, 150 and 200 mg/L) and pH (3.3, 6.84 and 10.8). It was found that the increasing of catalyst concentration enhanced the dye decolourisation. Hydrogen peroxide exerted positive effects on the AAB removal whilst the initial concentration of AAB negatively affected its removal. It was also found that the removal efficiency of AAB increased with the pH value close to neutral (pH 7), while a reversed trend was observed at acidic and basic medium.

KEY-WORDS: Photocatalytic, AOPs, catalyst, wastewater, H_2O_2 .

INTRODUCTION

Many modern techniques of treatment have been used over the last few decades to treat and purify water. Ozonation and photolysis techniques, for example, have been used successfully to degrade and reduce a range of organic and biological pollutants (Rice and Browning, 1981, Rice and Hoff, 1981, Barakat et al., 2005). However, stronger oxidant are produced (i.e. radicals) when these techniques are combined with some additives such as hydrogen peroxide and catalysts, and these processes together with additives are called Advanced Oxidation Processes (AOPs) (Glaze et al., 1987). AOPs are typically based on redox reactions as a result of gaining and losing electrons by radicals and organic molecules, respectively (Rice and Netzer, 1983). Among AOPs, in recent years, homogeneous photocatalysis methods have received a great attention in degrading or reducing organic pollutant (Al-Ekabi et al., 1991).

It is estimated that, in textile industries, more than 10 % of the dye is lost during the process of dyeing and discharged as effluent (Weber and Stickney, 1993). Since the existence of small quantities of dyes (even bellow 1 part per million) is clearly visible, the discharge of those coloured water pollutants in the environment is a considerable non aesthetic pollution source. Through hydrolysis, oxidation or other chemical reactions taking place in the phase of wastewater, wastes of dyes can also produce dangerous by-products and eutrophication (Zollinger, 1991, Tang et al., 1997). Therefore, dye effluents decolourisation has received

increasing attention. In liquid phase, addition of hydrogen peroxide (H_2O_2), as oxidant, is an accepted technique to accelerate photocatalytic oxidation. For photocatalytic oxidation of water phase, the hydrogen peroxide effect was extensively investigated. Addition of moderate H_2O_2 concentration was found to be significantly accelerate degradation of dyes and aromatic compounds (Barakat et al., 2005, Mart'yanov et al., 1997, Balcioglu and Inel, 1996, Dionysiou et al., 2004). This study outlines the results achieved for the degradation of acid alizarin black (AAB) in the presence of H_2O_2 . Various operating parameters were studied in this research including initial AAB concentration, amount of H_2O_2 and pH.

METHODOLOGY

Materials

Acid alizarin black (AAB) was purchased from Hopkin and Williams LTD, UK and used as received. A stock solution of AAB (1000 mg/L) was prepared on a daily basis in distilled water and other concentrations (100, 150 and 200 mg/L) were prepared by dilution the stock solution of AAB. The prepared stock solution was covered by aluminum foil and kept in dark. Hydrogen peroxide (H_2O_2) was purchased from ALPHA, India and used as received without further treatment. UV lamp with 254 nm (12 watt) was purchased from SEMTEC, China.

Experimental procedures

A closed semi-batch reactor, as shown in Fig. 1, was used in this study. A 500 mL, at a specific concentration, of the AAB solution was charged

into the reactor, this solution prepared from the stock solution by dilution. 30 % of H_2O_2 at a specific volume (0.1, 0.2 and 0.3 mL) was added to the AAB solution. The volume of the reactor was 600 mL. It is made from PYREX glass and fitted with a sample port. The reactor was equipped with a plunging tube in which a SEMTEC 12 watt lamp was placed horizontally.

A glass syringe with 5 mL volume was used, at a specific schedule, to collect samples. The pH values (3.23, 6.84, and 10.8) of these solutions were adjusted using 0.1M of NaOH and 0.1M of HNO_3 . The pH of the solution was determined using pH meter (EUTECH, Malaysia). Visible spectrophotometer (Jenway, 6700) was used to analyse the collected samples.

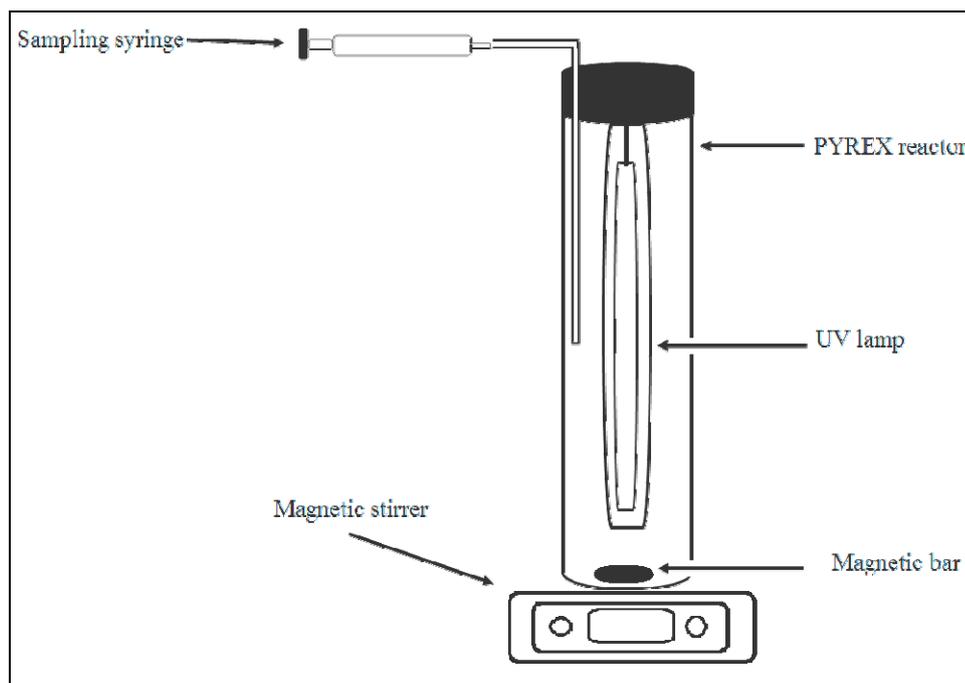


Fig. (1) Photocatalytic reactor

RESULTS AND DISCUSSION

The effect of H_2O_2 concentration on AAB decolourisation was studied and the results are shown in **Fig.2**. The figure shows the decolourisation of AAB solution in the presence of H_2O_2 . The other experiment conditions were kept constant (AAB concentration was set to 100 mg/L, pH 6.84, and room temperature $24^\circ C$). Various volume of H_2O_2 (0.1, 0.2 and 0.3 mL)

Effect of initial H_2O_2 concentration

were used. **Fig. 2** also shows how the increasing catalyst amount increases the removal efficiency. After 30 min reaction time, the decolourisation rate of AAB increased when the amount of H_2O_2 increased, due to the formation of highest amount OH^\bullet radicals when more H_2O_2 volume was used.

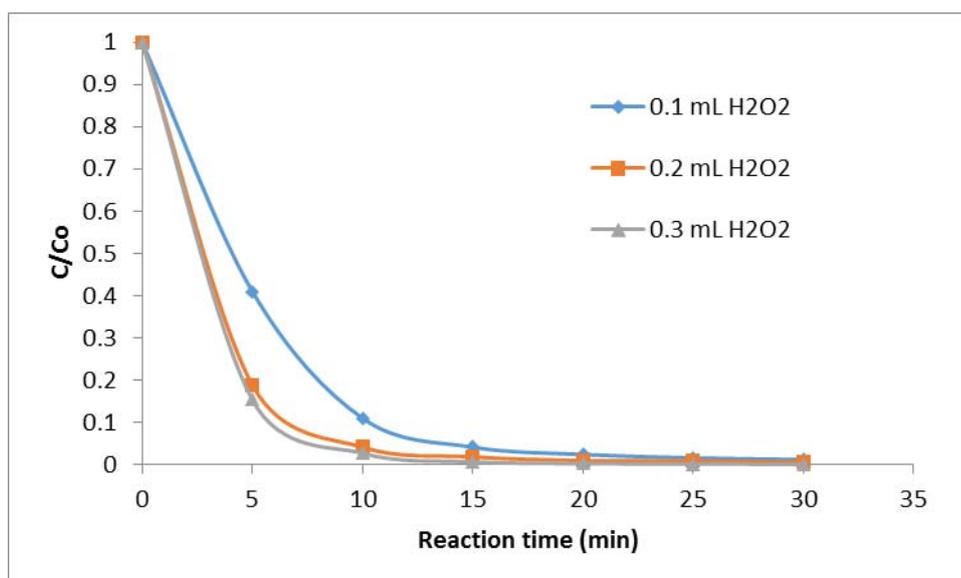


Fig. (2) AAB removal by using different amount of H_2O_2 at 30 min ($[AAB]_o = 100$ mg/L, Temperature= 24 °C, Volume = 500 mL, pH= 6.84)

After 5 min of the reaction (see **Fig. 3**), the removal percentage of AAB increased and reached 59 %, after using 0.1 mL of H_2O_2 . However, the removal percentage enhanced and reached 81 % and 84.5 % when the volume of

H_2O_2 increased to 0.2 and 0.3 mL, respectively. The removal efficiency of AAB was recorded the highest removal percentage when 0.3 mL of (H_2O_2) was used.

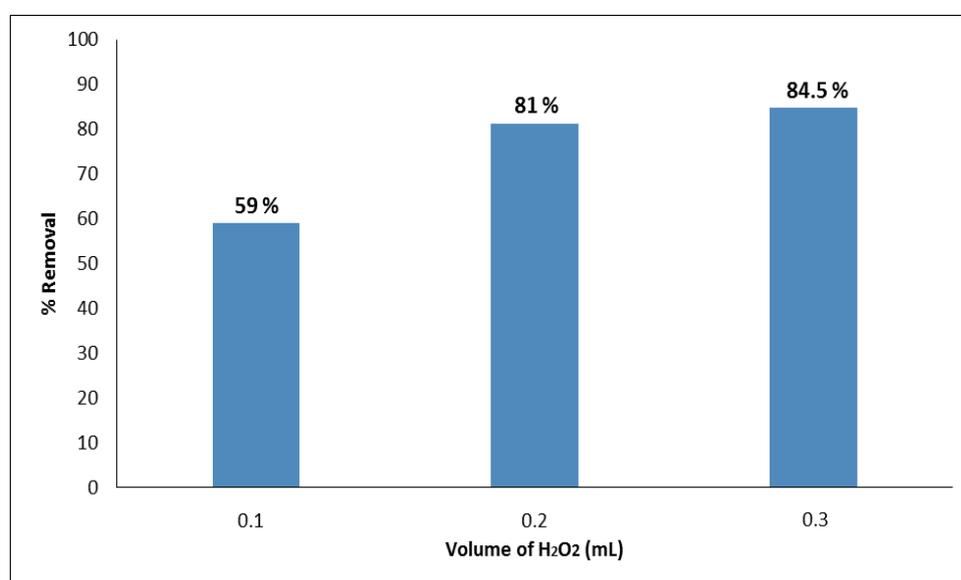


Fig. (3) AAB removal percentage at various amount of H_2O_2 at 5 min ($[AAB]_o = 100$ mg/L, Temperature= 24 °C, Volume = 500 mL, pH= 6.84)

Effect of initial AAB concentration

The effect of initial AAB concentration on the decolourisation rate of AAB was studied using UV light in the presence of H₂O₂. The results show that increasing the initial concentration of AAB reduced the decolourisation rate (see Fig. 4). The rate constant, k' , was found to decrease linearly with increased initial AAB concentration. When AAB concentration increased from 100 to 200 mg/L, the decolourisation percentage of AAB at 5 min reaction time decreased from 81 % to 21 %, respectively (see Fig. 5). The dye loss, according to the following equation, was observed as a function of time and data were fitted to a pseudo first order rate model (Bali et al., 2004, Esplugas et al., 2002).

$$\ln\left(\frac{C}{C_0}\right) = -k't$$

The plot of $\ln(C/C_0)$ versus time gives a straight line with $k' = -\text{slope}$ (k' , as seen from figure, depends on the H₂O₂ concentration), so the reaction follows a pseudo-first order scheme. Table 1 and Table 2 show the effect of dye concentration and amount of H₂O₂ on rate constant.

Table (1): Effect of AAB concentration on a pseudo-first order kinetic for the degradation of AAB

[AAB] (mg/L)	k' (min ⁻¹)	R ²
100	0.2483	0.9608
150	0.1511	0.9808
200	0.0844	0.994

Table (2): Effect of H₂O₂ amount on a pseudo-first order kinetic for the degradation of AAB

H ₂ O ₂ Volume (mL)	k' (min ⁻¹)	R ²
0.1	0.1953	0.984
0.2	0.2327	0.9608
0.3	0.3052	0.9865

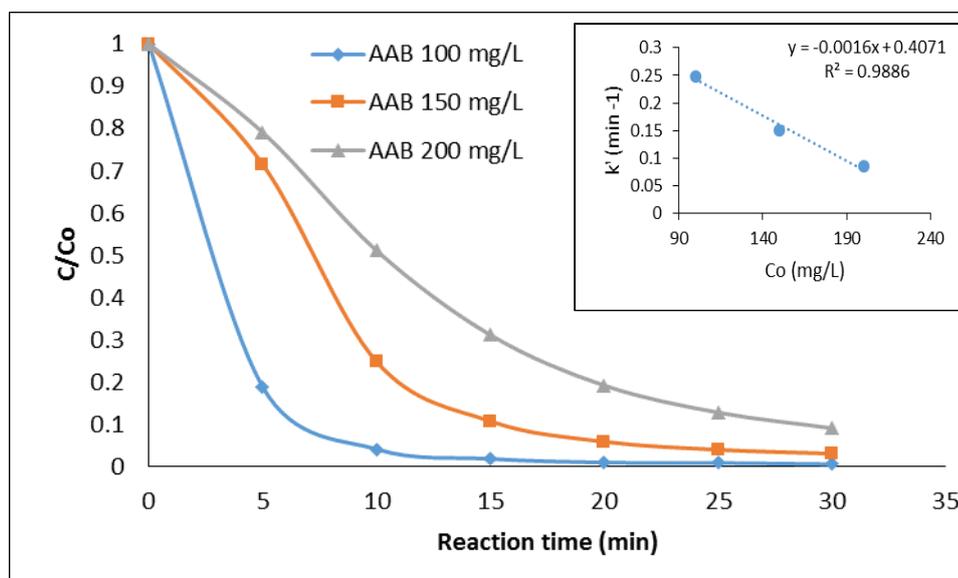


Fig. (4): Effect of initial AAB concentration on solution decolourisation at 60 min (Temperature= 23 °C, Volume= 500 mL, pH= 6.84)

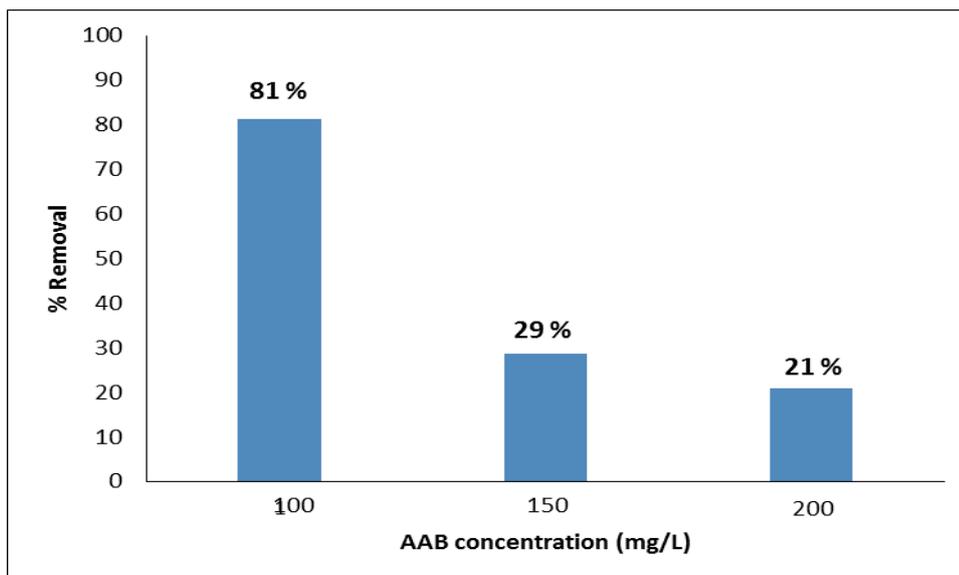


Fig. (5) AAB removal percentage at various concentrations of AAB at 5 min (Temperature= 23 °C, Volume = 500 mL, pH= 6.84)

Effect of pH

The process of AAB removal is higher at pH close to 7 compared to AAB removal in acidic and basic medium. As shown in **Fig. 6**, the removal percentage improved from 94 to 97

% when pH changed from 3.3 to 6.84, respectively. However, the improvement decreased from 97 to 95.4 % when pH increased from 6.84 to 10.8, respectively.

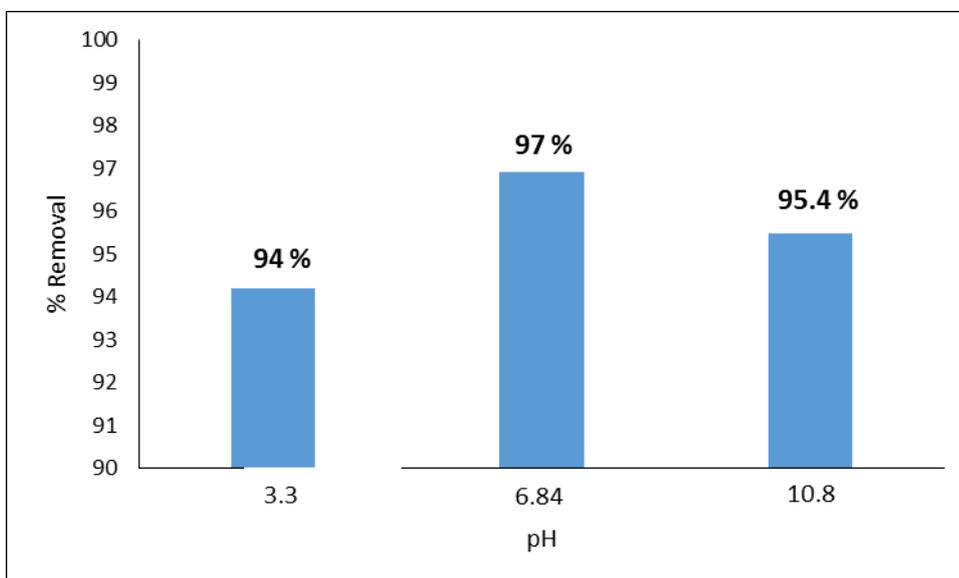


Fig. (6) Effect of pH on AAB removal percentage at 30 min (Temperature= 23 °C, Volume = 500 mL)

CONCLUSIONS

Photocatalytic degradation, in the presence of H₂O₂, of AAB under different operating conditions was studied in this research. The operating conditions were initial dye concentration, amount of H₂O₂ and pH. The most effective improvements on the degradation of AAB were recorded with initial AAB concentration of 100 mg/L. It was also found that the increasing of H₂O₂ quantity enhance the reaction rate of AAB decolourisation. The removal efficiency of AAB was favourable in the neutral medium more than the acidic and basic medium. The removal percentage reached the maximum value at pH close to 7.

REFERENCES

- AL-EKABI, H., SAFARZADEH-AMIRI, A., SIFTON, W. & STORY, J. 1991. Advanced technology for water purification by heterogeneous photocatalysis. *International Journal of Environment and Pollution*, 1, 125-136.
- BALCIOGLU, I. A. & INEL, Y. 1996. Photocatalytic degradation of organic contaminants in semiconductor suspensions with added H₂O₂. *Journal of Environmental Science and Health - Part A Environmental Science and Engineering and Toxic and Hazardous Substance Control*, 31, 123-138.
- BALI, U., ÇATALKAYA, E. & ŞENGÜL, F. 2004. Photodegradation of Reactive Black 5, Direct Red 28 and Direct Yellow 12 using UV, UV/H₂O₂ and UV/H₂O₂/Fe²⁺: a comparative study. *Journal of Hazardous Materials*, 114, 159-166.
- BARAKAT, M. A., TSENG, J. M. & HUANG, C. P. 2005. Hydrogen peroxide-assisted photocatalytic oxidation of phenolic compounds. *Applied Catalysis B: Environmental*, 59, 99-104.
- DIONYSIOU, D. D., SUIDAN, M. T., BAUDIN, I. & LAÏNÉ, J. M. 2004. Effect of hydrogen peroxide on the destruction of organic contaminants-synergism and inhibition in a continuous-mode photocatalytic reactor. *Applied Catalysis B: Environmental*, 50, 259-269.
- ESPLUGAS, S., GIMÉNEZ, J., CONTRERAS, S., PASCUAL, E. & RODRÍGUEZ, M. 2002. Comparison of different advanced oxidation processes for phenol degradation. *Water Research*, 36, 1034-1042.
- GLAZE, W. H., KANG, J. W. & CHAPIN, D. H. 1987. The Chemistry of Water Treatment Processes Involving Ozone, Hydrogen Peroxide and Ultraviolet Radiat. *International Ozone Association*, 9, 335-352.
- MARTYANOV, I. N., SAVINOV, E. N. & PARMON, V. N. 1997. Photocatalytic Oxidation of Methyl Viologen in an Aqueous Suspension of TiO₂ in the Presence of Oxygen and Hydrogen Peroxide. The Effect of the Solution pH and H₂O₂ Concentration on the Reaction Rate. *Kinetics and Catalysis*, 38, 70-76.
- RICE, E. W. & HOFF, J. C. 1981. Inactivation of Giardia lamblia cysts by ultraviolet irradiation. *Appl Environ Microbiol*, 42, 546-7.
- RICE, R. G. & BROWNING, M. E. 1981. *Ozone treatment of industrial wastewater*, Park Ridge, N.J., Noyes Data Corp.
- RICE, R. G. & NETZER, A. 1983. Handbook of Ozone Technology and Applications, Vol 1, Rice, Rg, Netzer, A. *Journal American Water Works Association*, 75, 64-64.
- TANG, W. Z., ZHANG, Z., AN, H., QUINTANA, M. O. & TORRES, D. F. 1997. TiO₂/UV photodegradation of azo dyes in aqueous solutions. *Environmental Technology*, 18, 1-12.
- WEBER, E. J. & STICKNEY, V. C. 1993. Hydrolysis kinetics of Reactive Blue 19-Vinyl Sulfone. *Water Research*, 27, 63-67.
- ZOLLINGER, H. 1991. *Color chemistry: syntheses, properties, and applications of organic dyes and pigments*, VCH.

تیکچوونا بویاغا ترشی ئەلیزارینی رهش بریکه هاندهری روناھیی ب کارئینانا ژوور ئوکسیدی هایدروجین

پوخته:

دقیقە کولینیدا تیکچوونا بویاغا ترشی ئەلیزارینی رهش (AAB, C.I. 21725) بریکه هاندهری روناھیی هاته کرن دناؤ ئاویته کی ئافی دا بکارئینانا تیشکا سهه بنهفشیدا وب ههبوونا ژوور ئوکسیدی هایدروجین (H_2O_2) وهک کاریگهه کی هاندهر لب جنه کرداریت جیاواز. باردوخین کاری بین قی قه کولینی پینک دهاتن (0.3, 0.2, 0.1 ملیلتر ژ 30% H_2O_2) ژپهیتی کاریگهه دیگهل پهیتی سهههتایی ب (100, 150, 200 ملغم/ لتر) بی بویاغا AAB و pH ی ئاویتهی (3.3, 6.84, 10.8). هاته دیتن ژقی قه کولینی ب زنده کرنا پهیتی هاندهری هاریکاریی دکهت لسهه ژیرنا رهنگی بویاغا AAB. هاندهری ژوور ئوکسیدی هایدروجینی هندهک ئەنجامین پوزه تیشقانه دان لسهه ژیرنا بویاغا AAB لی ب بکارئینانا پهیتی سهههتایی بی AAB کارتیکر نه کا نیکیتیفانه کر لسهه ژیرنا قی بویاگی. ههروهسا هاته دیتن ئەف هاندهره دشیته ژیرنا بویاغا AAB زنده کته دکهل بهایی pH نیریک بیت بو هاوتا (pH 7)، به لی دی دیار بیت بیچه وانه به دناقه ندا ترش و تفتی دا.

تدهور التحفيز الضوئي لصبغة حامض أليزارين الأسود باستخدام بيروكسيد الهيدروجين

الخلاصة

تم دراسة تدهور التحفيز الضوئي لصبغة حامض أليزارين الأسود (AAB, C.I. 21725) في المحلول المائي باستخدام الأشعة فوق البنفسجية وبوجود بيروكسيد الهيدروجين (H_2O_2) كعوامل محفزة في حالة ظروف مختلفة. وكانت ظروف العمل لهذه الدراسة هي (0.1, 0.2, 0.3 مليلتر من 30% H_2O_2) لجرعة الخفض والتكيز الأولي (100, 150, 200 ملغم/ لتر) لصبغ ال AAB و pH المحلول (3.3, 6.84, 10.8). وقد وجد في هذه الدراسة أن زيادة تركيز المحفز يعزز من إزالة اللون لصبغة AAB. بيروكسيد الهيدروجين أعطت نتائج إيجابية في إزالة صبغة ال AAB في حين أن التركيز الأولي ل AAB تأثرت سلباً في إزالة هذه الصبغة. تبين أيضاً أن كفاءة إزالة صبغة ال AAB زادت مع قيمة pH قريباً إلى متعادل (pH 7)، في حين لوحظ السلوك العكسي في الوسط الحامضي و القاعدي.